PATENT APPLICATION

10072-US-PCT

In the Claims:

Cancel Claim 26.

Amend Claim 4 to read:

4 (currently amended). A process for the esterification of a dicarboxylic acid compound and an

alcohol compound comprising contacting a process feed comprising a dicarboxylic acid

compound and an alcohol compound with the catalyst complex comprising:

i) a polymeric titanium glycolate represented by the formula [TiO<sub>4</sub>(CH<sub>2</sub>)<sub>4</sub>]<sub>n</sub> wherein n is 8 to 200

and is not soluble in ethylene glycol; and

ii) an alkali metal glycolate,

wherein the molar ratio of the polymeric titanium glycolate and the alkali metal glycolate is 1.25:1

to 100:1,

wherein the total content of the metals of the catalyst is from 1 to 70 ppm based on the esterification

component,

wherein the dicarboxylic acid compound is represented by the formula HOOC-R-COOH,

wherein R is a linear or branched alkyl, alkenyl or aryl group containing 2 to 30 carbon atoms.

Amend Claim 25 to read:

25 (currently amended). The process according to claim 24 4, wherein the polymeric titanium

glycolate is soluble in an alkali metal glycolate.

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#### LISTING OF CLAIMS IN THE APPLICATION

- 1. Canceled
- 2. Canceled
- 3. Canceled
- 4 (currently amended). A process for the esterification of a dicarboxylic acid compound and an alcohol compound comprising contacting a process feed comprising a dicarboxylic acid compound and an alcohol compound with the catalyst complex comprising:
- i) a polymeric titanium glycolate represented by the formula [TiO<sub>4</sub>(CH<sub>2</sub>)<sub>4</sub>]<sub>n</sub> wherein n is 8 to 200 and is not soluble in ethylene glycol; and
- ii) an alkali metal glycolate,

wherein the molar ratio of the polymeric titanium glycolate and the alkali metal glycolate is 1.25:1 to 100:1,

wherein the total content of the metals of the catalyst is from 1 to 70 ppm based on the esterification component,

wherein the dicarboxylic acid compound is represented by the formula HOOC-R-COOH, wherein R is a linear or branched alkyl, alkenyl or aryl group containing 2 to 30 carbon atoms.

5 (previously presented). The process according to claim 4, wherein R contains 4 to 15 carbon

atoms.

6 (previously presented). The process according to claim 5, wherein the dicarboxylic acid

compound is selected from the group consisting of terephthalic acid, isophthalic acid,

naphthalenic diacid, succinic acid, adipic acid, phthalic acid, glutaric acid, oxalic acid and maleic

acid.

7 (previously presented). The process according to claim 6, wherein the dicarboxylic acid

compound is terephthalic acid.

8 (previously presented). The process according to claim 4, wherein the dicarboxylic acid

compound is an oligomer having repeating units derived from a carboxylic acid.

9 (previously presented). The process according to claim 4, wherein the alcohol compound

comprises an alkylene glycol represented by the formula HO-R'-OH or a polyalkylene glycol

represented by the formula HO-[R"-O-]<sub>n</sub>-H, wherein R' is a linear or branched alkyl group,

having 2 to 10 carbon atoms, and wherein R" is an alkyl group having 1 to 10 carbon atoms.

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10 (previously presented). The process according to claim 6, wherein the alcohol compound is

selected from the group consisting of ethylene glycol, propylene glycol, isopropylene glycol,

butylene glycol, 1-methyl propylene glycol, pentylene glycol, neopentylene glycol, and

combinations thereof.

11 (previously presented). The process according to claim 4, wherein the process is carried out

at a temperature of 150°C to about 500°C and at a pressure of about 0.001 atmosphere to about

10 atmospheres.

12 (previously presented). The process according to claim 10, wherein the process is carried out

at a temperature of about 250°C to about 300°C and a pressure of about 0.001 atmospheres to

about 10 atmospheres.

13 (previously presented). The process according to claim 4, wherein the molar ratio of the

alcohol compound to the dicarboxylic acid compound is in the range of about 0.1:1 to about

10:1.

14 (previously presented). The process according to claim 10, wherein the catalyst complex is

present in a concentration of about 1 ppm to about 70 ppm in the process feed.

15. Canceled

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### 16. Canceled

17 (previously presented). The process according to claim 7, wherein the alcohol compound comprises ethylene glycol.

18 (previously presented). The process according to claim 10, wherein the molar ratio of the alcohol compound to the dicarboxylic compound in the process feed is in the range of about 1:1 to about 3:1.

19 (previously presented). The process according to claim 4, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.

20 (previously presented). The process according to claim 9, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.

21 (previously presented). The process according to claim 12, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.

## 22. Canceled

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23 (previously presented). The process according to claim 4, wherein the total content of metals of the catalyst is from 10 ppm to 50 ppm.

## 24. Canceled

25 (currently amended). The process according to claim 24 4, wherein the polymeric titanium glycolate is soluble in an alkali metal glycolate.

# 26. Canceled